

# DNS of a Turbulent Boundary Layer with Passive Scalar Transport



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# Outline

- Introduction
  - Motivation
  - Basic Concepts
  - Purposes
- Direct Numerical Simulation (DNS)
- Results
- Conclusions & Outlook



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# Motivation

Basic understanding of wall-bounded turbulence:

- Crucial in engineering applications: external flows, e.g. turbine blades, vehicles, airfoils etc.
- Need for spatial simulations at moderate to high Re

Passive scalar mixing (e.g. heat transfer):

- Understanding of the passive scalar transport is limited (Reynolds analogy etc.)
- Quantities that cannot be measured in a wind tunnel or other experimental facilities (budgets, dissipation, h.o.t. etc.)
- Clearly a lack of fully-resolved numerical simulations (DNS) in boundary layer with passive scalar
- Applications in cooling, pollutant dispersion, combustion, heat exchanger



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# Basic Concepts

- Boundary layer  
Ludwig Prandtl in 1905
- Passive scalar  
diffusive contaminant  
low concentration: small amounts of heat or pollutant
- Molecular Prandtl number  $Pr = \frac{\nu}{\alpha}$   
 $\nu$  is the kinematic viscosity  
 $\alpha$  the scalar molecular diffusivity

large  $Pr \implies$  convection is effective

small  $Pr \implies$  conduction is effective

	air	water	oil	mercury
$Pr$	0.71	7	100-40000	0.025

values from White (2006)



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# Purposes

- Implement a huge variety of low and higher-order statistics, two-point correlations and time signals in the code (SIMSON)
- Perform a DNS to extend our knowledge of  $Re$  and  $Pr$  effects on the turbulence velocity and scalar statistics
- Based on the DNS results to develop new SGS models for scalars
- Generate a database for research community



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# Outline

- Introduction

- Direct Numerical Simulation (DNS)

- Governing Equations
- Numerical Scheme
- Computational Domain
- Boundary Conditions
- Main Parameters

- Results

- Conclusions & Outlook



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# Governing Equations

- Incompressible Navier-Stokes equation  
→ good approximation for low-speed flows ( $Ma < 0.3$ )

$$\frac{\partial u_i}{\partial t} + u_j \frac{\partial u_i}{\partial x_j} = -\frac{\partial p}{\partial x_i} + \frac{1}{Re} \frac{\partial^2 u_i}{\partial x_j \partial x_j}$$

- Continuity equation

$$\frac{\partial u_i}{\partial x_i} = 0$$

- Scalar transport equation

$$\frac{\partial \theta}{\partial t} + u_i \frac{\partial \theta}{\partial x_i} = \frac{1}{RePr} \frac{\partial^2 \theta}{\partial x_i \partial x_i}$$

$$Re = \frac{U_\infty \delta_0^*}{\nu}, Pr = \frac{\nu}{\alpha}, Pe = RePr$$

- Solved by DNS → all scales are resolved, terms are evaluated without modelling → expensive
- Memory  $\sim Re^{9/4}$  and CPU time  $\sim Re^3$



# Numerical Scheme



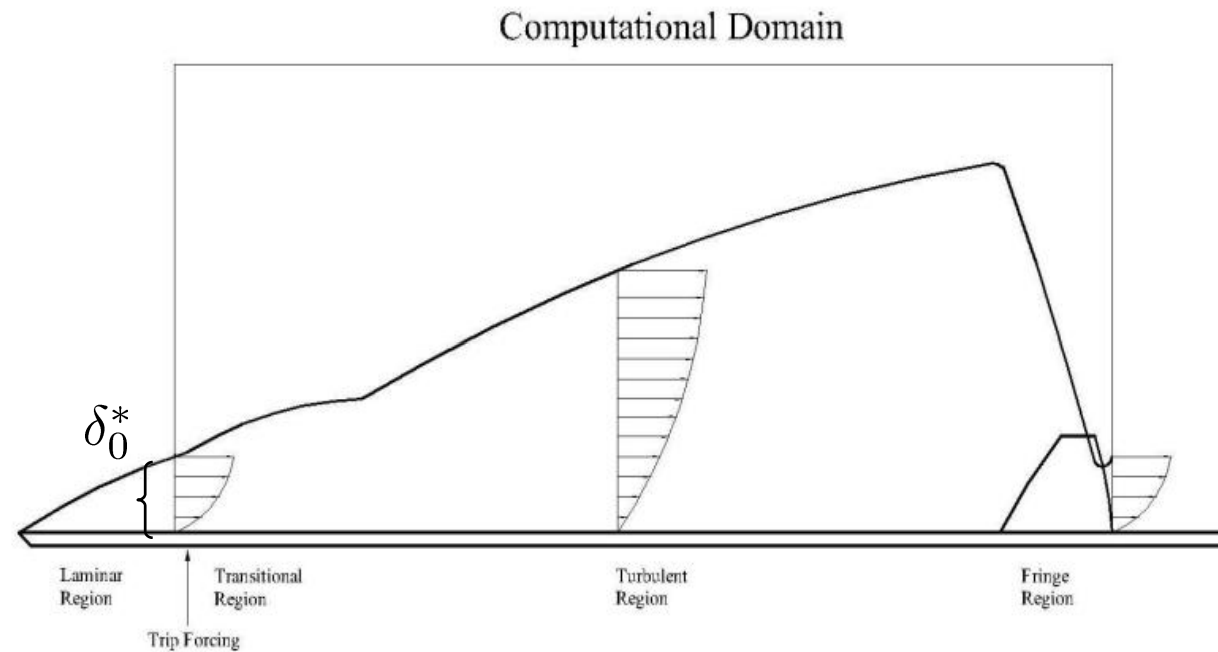
- Code SIMSON, developed at KTH Mekanik, Reference: Chevalier et al. (2007)
- Spatial Discretization (Fully spectral)
  - Horizontal directions
    - Fourier expansions → Periodic B.C.
  - Wall-normal direction
    - Chebyshev expansions
- Time Advancement
  - linear terms
    - 2nd-order Crank-Nicolson method
  - Non-linear terms
    - 3rd-order 4-step Runge-Kutta method



# Computational Domain



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- Domain does not include leading edge
- Laminar inflow, tripped by random forcing
- Fringe region at the end
- No-slip at the wall, Neumann on top

# Boundary Conditions

- Scalar Field
  - Lower boundary condition

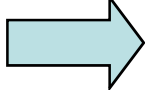
$$\theta|_{y=0} = 0, \text{ for the isothermal boundary condition}$$

$$\left. \frac{\partial \theta}{\partial y} \right|_{y=0} = 1, \text{ for the isoflux boundary condition}$$

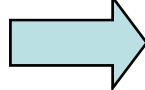
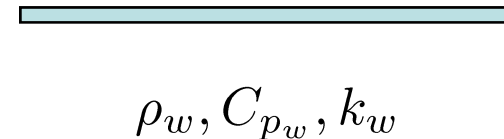
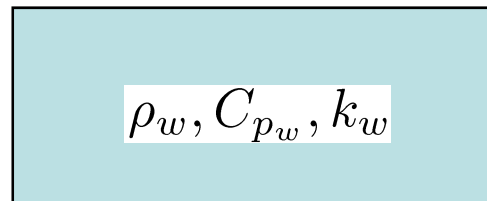
- Upper boundary condition

$$\theta|_{y=y_L} = 1$$

$\rho, C_p, k$



$\rho, C_p, k$

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## Main Parameters

$Re_x$	68450-315950
$Re_{\delta^*}$	450-1234
$Re_{\theta}$	175-830
$Re_{\delta_{99}}$	46-316
geometry ( $\delta_0^*$ )	$750 \times 40 \times 34$
fringe start $x_{start}$	660
fringe end $x_{end}$	750
fringe strength $\lambda_{max}$	1.0
$\Delta_{rise}$	50
$\Delta_{fall}$	15
resolution	$1024 \times 289 \times 128$
grid spacing in $x$ ( $\Delta x^+$ )	17
grid spacing in $y$ ( $\Delta y^+$ )	0.025-4.6
grid spacing in $z$ ( $\Delta z^+$ )	6.3

+ viscous units

CPU time  $\rightarrow$  5 months



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# Outline

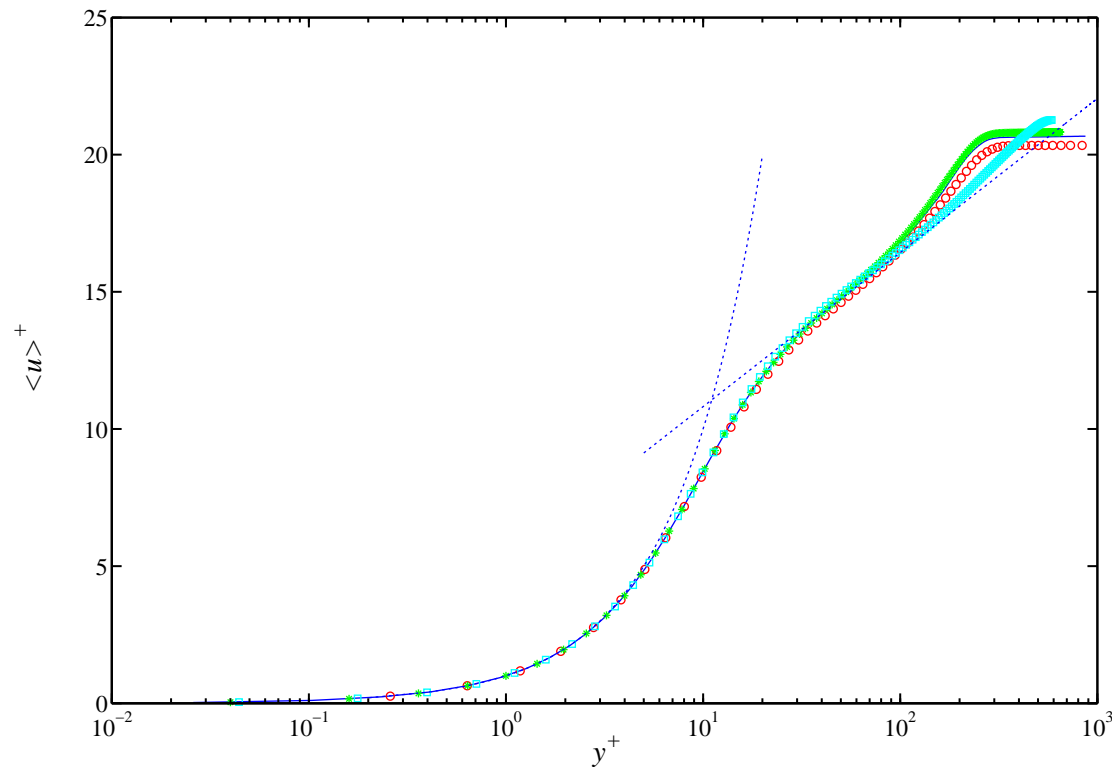
- Introduction
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  - Hydrodynamic Results
  - Scalar Transport Results
  - Comparison between the Two Fields
- Conclusions & Outlook



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# Hydrodynamic Results

Mean Velocity Profile at  $Re_\theta = 670$



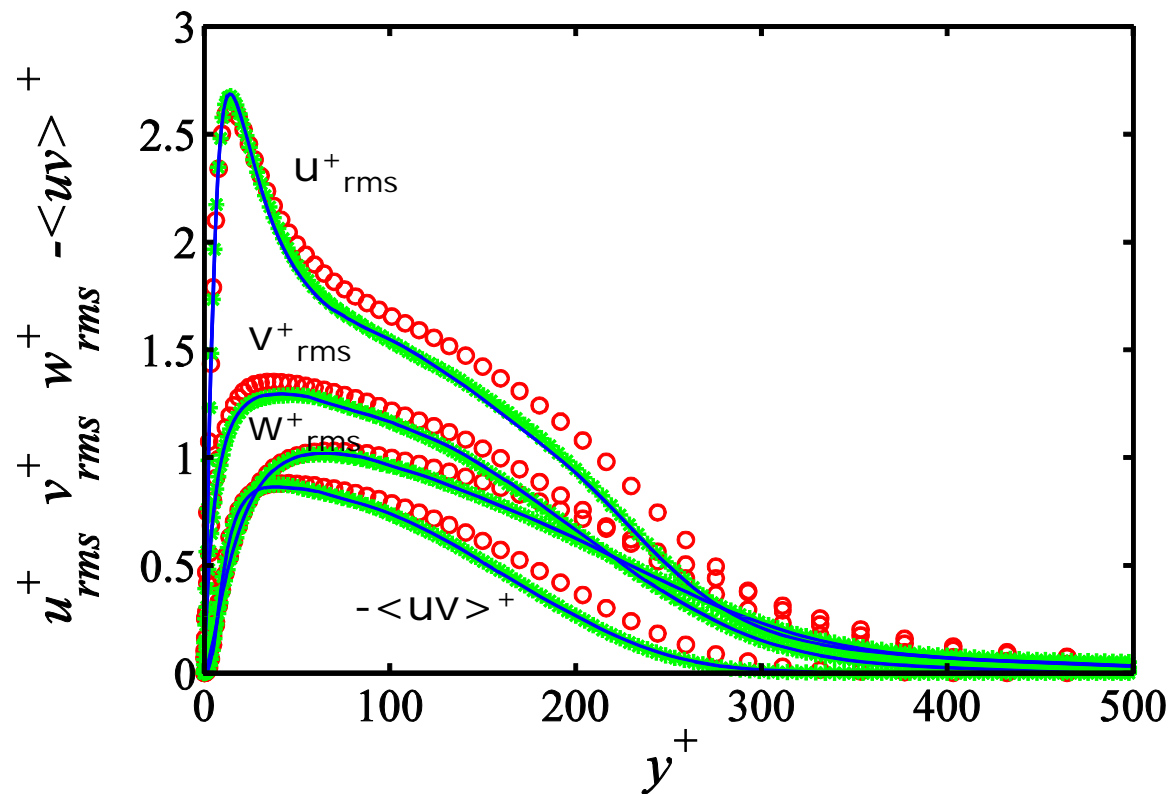
- $Re_\theta = 670$  Spalart (1988), \*  $Re_\theta = 666$  Komminaho and Skote (2002),
- $Re_\tau = 590$  Moser et al. (1999), ... Log-law
  - good agreement in log region and with log-law
  - wake region only for BL cases



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# Hydrodynamic Results

Turbulent Intensities at  $Re_\theta = 670$



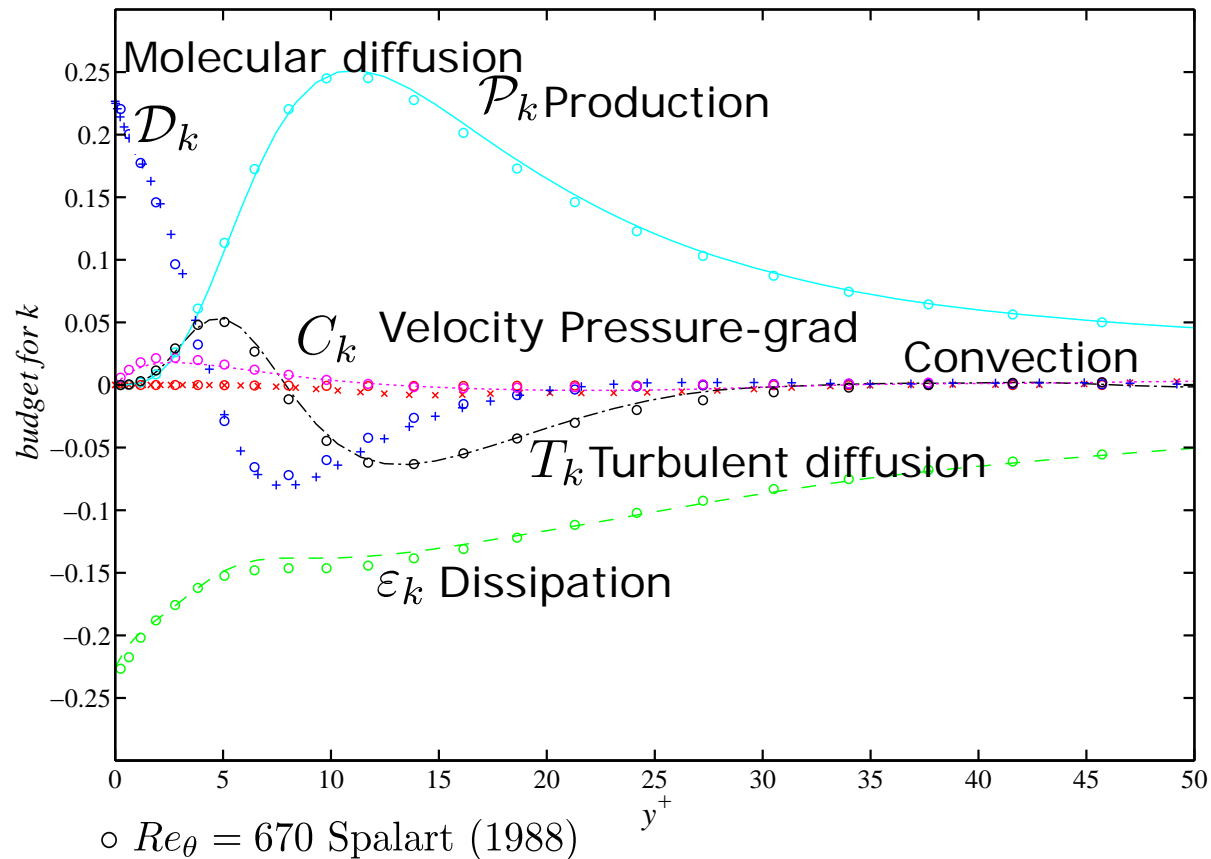
○  $Re_\theta = 670$  Spalart (1988), \*  $Re_\theta = 666$  Komminaho and Skote (2002)



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# Hydrodynamic Results

Budget for kinetic energy  $k = \frac{1}{2} \langle u'_i u'_i \rangle$  at  $Re_\theta = 670$



# Scalar Transport Results

A list of scalars in the present DNS

scalar	boundary condition	$Pr$
$\theta_1$	isothermal	0.2
$\theta_2$	isothermal	0.71
$\theta_3$	isoflux	0.71
$\theta_4$	isothermal	2.0
$\theta_5$	isoflux	2.0



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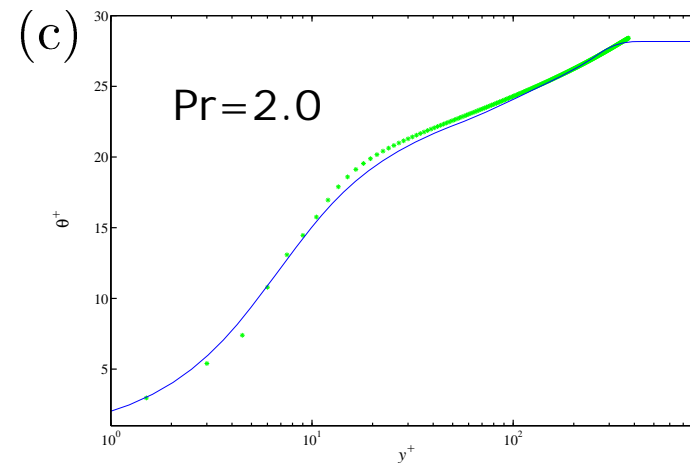
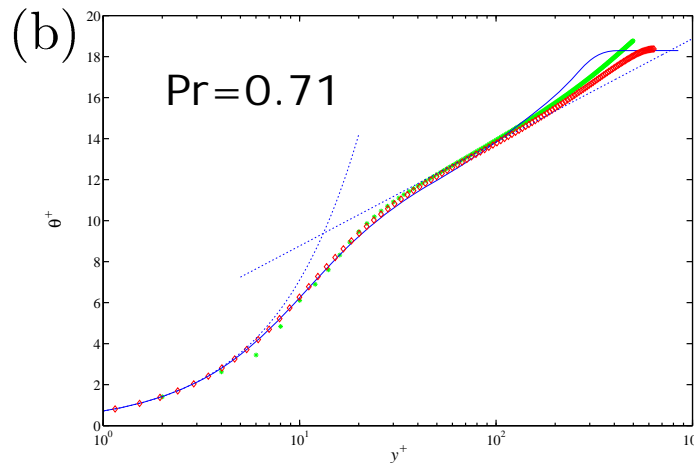
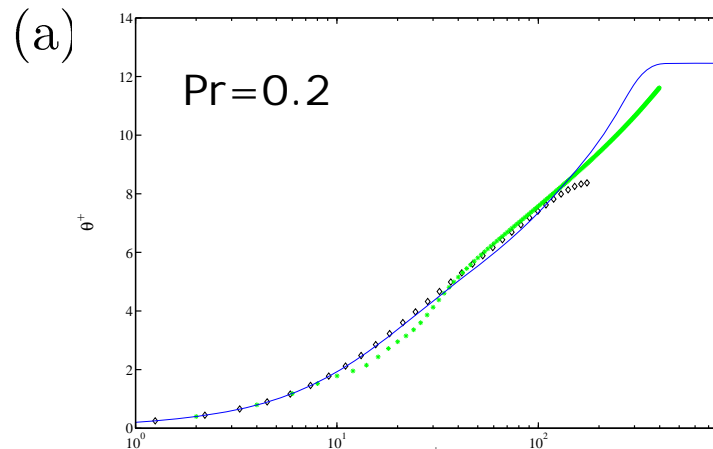


# Scalar Transport Results

Mean Scalar Profiles at  $Re_\theta = 830$



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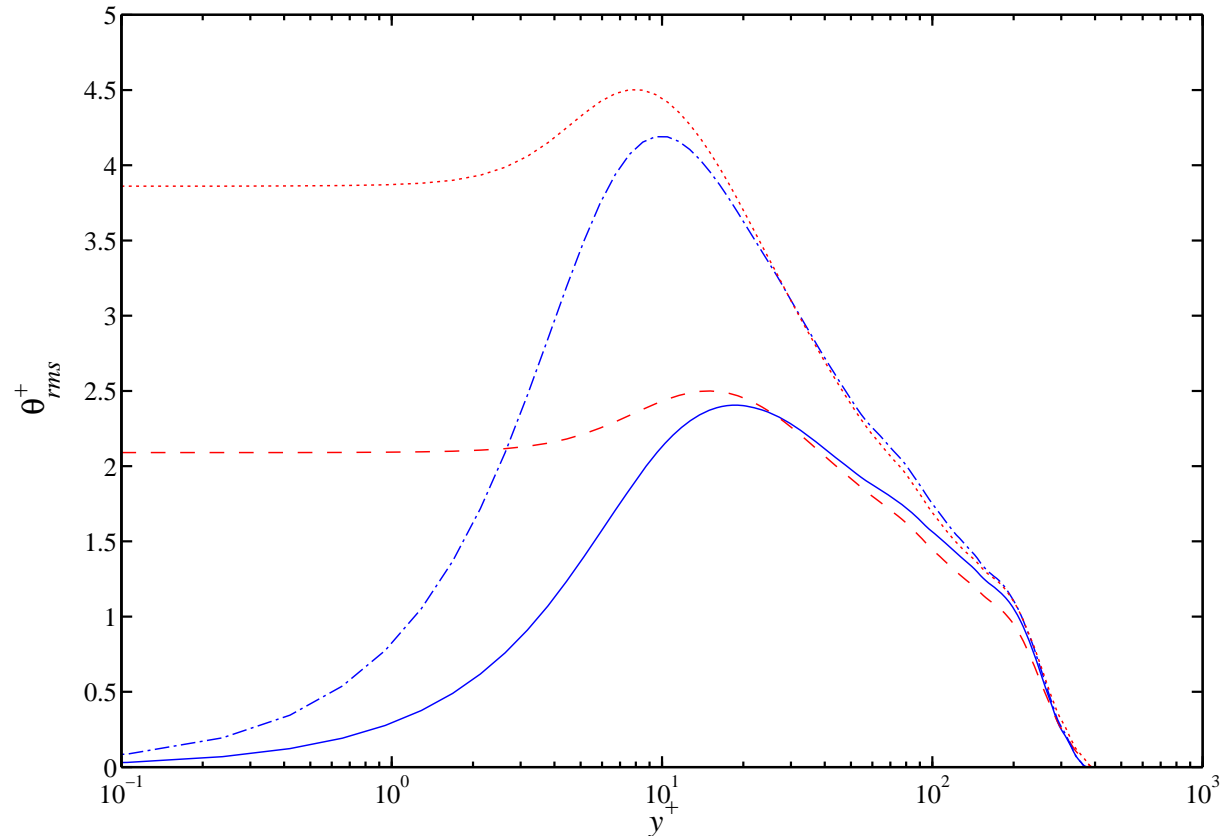


(a) $\theta_1$ , (b) $\theta_2$ , (c) $\theta_4$ , \* Kader (1981),  $\diamond$   $Re_\tau = 640$  Abe et al. (2004)

$\diamond$   $Re_\tau = 180$  Kawamura et al. (1998), b.c. no difference

# Scalar Transport Results

Comparisons between different boundary conditions at  $Re_\theta = 830$



—  $\theta_2$ , - -  $\theta_3$ , - · -  $\theta_4$ , ···  $\theta_5$

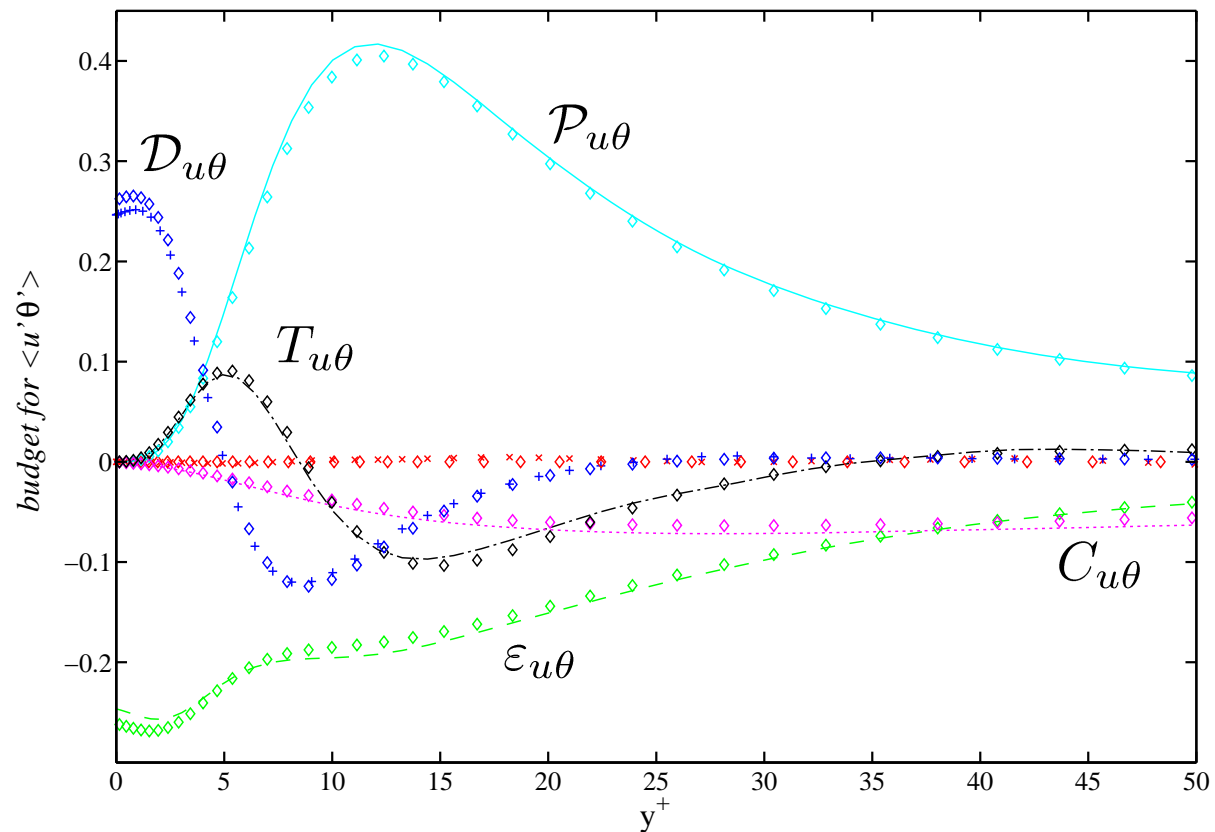
- non-zero at the wall and constant very near the wall
- far away, no difference



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# Scalar Transport Results

Budget for streamwise scalar flux  $\langle u'\theta' \rangle$  of  $\theta_2$  at  $Re_\theta=830$

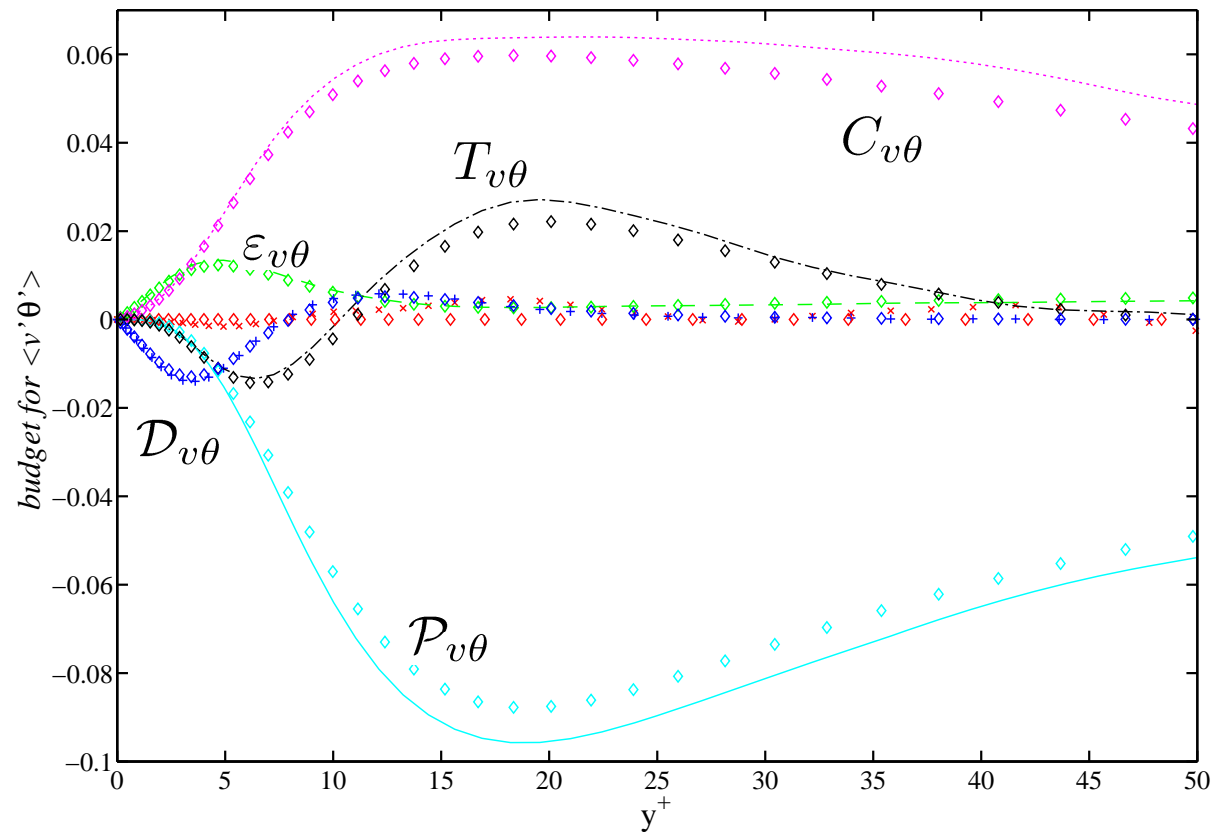


$\diamond Re_\tau = 395$  Abe et al. (2004)



# Scalar Transport Results

Budget for wall-normal scalar flux  $\langle v'\theta' \rangle$  of  $\theta_2$  at  $Re_\theta=830$

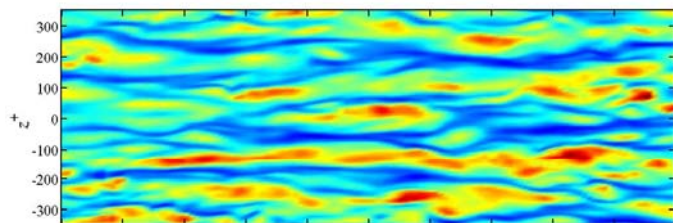
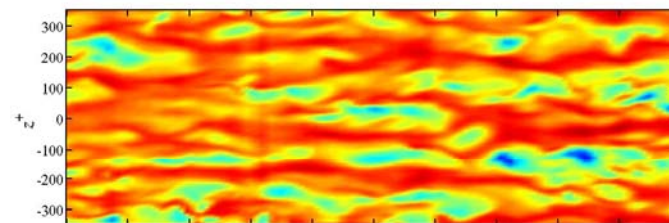
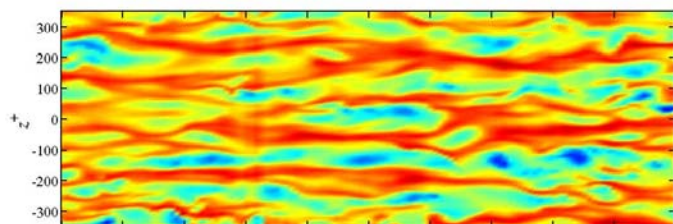
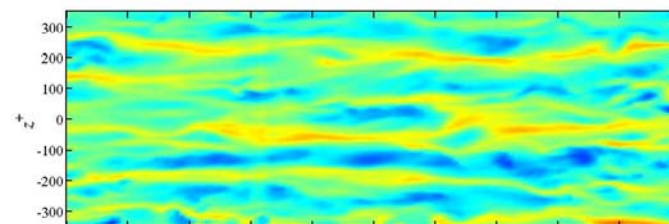
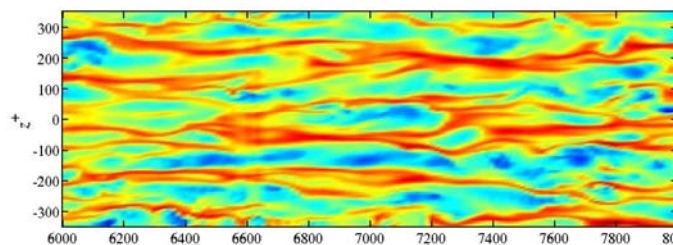
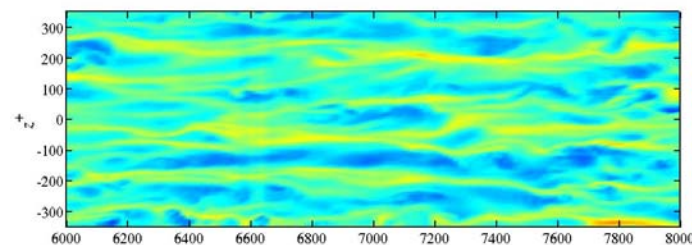


$\diamond Re_\tau = 395$  Abe et al. (2004)



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## Instantaneous Fields

(a)  $u'$  at  $y^+ \approx 7$ (b)  $\theta'_1$  at  $y^+ \approx 7$ (c)  $\theta'_2$  at  $y^+ \approx 7$ (d)  $\theta'_3$  at  $y^+ \approx 7$ (e)  $\theta'_4$  at  $y^+ \approx 7$ (f)  $\theta'_5$  at  $y^+ \approx 7$ 

same time,  $x^+ = 6000 - 8000$ ,  $Re_\theta = 570 - 680$ ,  $\Delta z^+ \approx 750$



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# Conclusions

- A DNS of turbulent boundary layer flow has been performed with five different scalars.  $Re$  is higher than the previously available DNS
- In general, comparisons with other DNS data are very good
- In the near-wall region boundary layer and channel simulations are very similar, however distinct differences are visible in the outer region
- The effect of the boundary condition is confined to the near-wall region



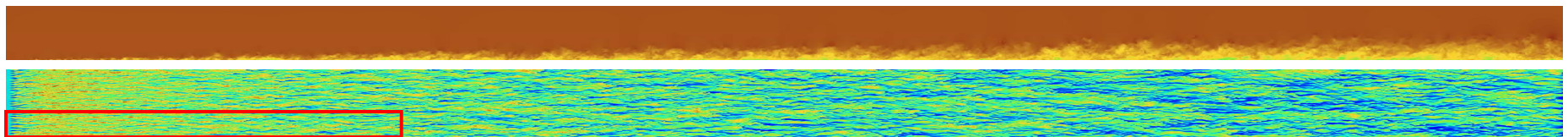
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# Outlook

- Larger box to reach higher Re
- Higher or lower Pr: different grids for the two fields
- Active scalar, Boussinesq approximation
- Free-stream turbulence (FST), bypass transition, Reynolds analogy in the presence of FST
- Validation of LES: SGS modeling of the scalar field



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$1.5 \times 10^9$  grid points reaching  $Re_\theta = 2500$   
→ Compare with experiments





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Thank you!